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PROVISIONAL APPLICATION COVER SHEET

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ALDEHYDE AND ALCOHOL COMPOSITIONS DERIVED FROM SEED OILS					
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			Docket Number	63104
TITLE OF THE INVENTION (280 characters max)				
ALDEHYDE AND ALCOHOL COMPOSITIONS SERIVED FROM SEED OILS				
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ALDEHYDE AND ALCOHOL COMPOSITIONS DERIVED FROM SEED OILS

In one aspect, this invention pertains to aldehyde and alcohol compositions, preferably, derived from seed oils. In another aspect, this invention pertains to a process of preparing the aldehyde composition via hydroformylation of an unsaturated fatty acid or unsaturated fatty acid ester feedstock derived from seed oils. Likewise, this invention also pertains to a process of preparing the alcohol composition via hydroformylation and subsequent hydrogenation of an unsaturated fatty acid or unsaturated fatty acid ester feedstock derived from seed oils.

Alcohol compositions are useful in that they can be converted into polyols that find utility in the manufacture of polyurethanes. Aldehyde compositions are useful in that they can be converted via hydrogenation into alcohols or amines, which in turn can be converted into polyols and polyamines for the manufacture of polyurethanes. Aldehydes can also be converted into carboxylic acids, hydroxy acids, amino alcohols, amino acids, and other commercially useful derivatives.

Currently, industry-wide efforts are underway to replace petroleum-based chemical feedstocks with non-petroleum-based chemical feedstocks. Seed oils, which comprise a mixture of saturated and unsaturated fatty acid esters, provide a promising source of renewable non-petroleum-based feedstocks for industrial utilization. Aldehydes and alcohols derived from seed oils have the potential to be converted into many useful industrial chemicals, notably, polyols for use in polyurethanes.

To be useful in polyurethane manufacture non-petroleum-based polyols should provide for similar reactivity and urethane end-product at acceptable cost, as compared with conventional petroleum-based polyols. Non-petroleum-based polyols may also provide opportunities for preparing unconventional polyurethane products having novel properties. The properties of polyurethanes are known to vary depending upon the polyol composition employed during polyurethane manufacture. Non-petroleum-based aldehyde and alcohol compositions should be engineered such that the polyols derived therefrom yield polyurethanes of acceptable properties for their desired end-use. Polyols to be used in manufacture of polyurethane slab stock flexible foams, for example, should provide for acceptable cross-link density, that is, cross-link density neither too high nor too low, else the foam has unacceptable rigidity or flexibility. The invention described herein pertains

particularly to aldehyde and alcohol compositions that are preferably derived from seed oils and that provide for polyols having acceptable properties for the manufacture of polyurethane slab stock flexible foams.

Prior art, as exemplified by US 3,787,459, discloses a process for converting
5 unsaturated vegetable oil materials via hydroformylation into formyl (aldehyde) products. Disclosed vegetable oils include soybean, linseed, and safflower oils, and their derivatives. Typically, the process appears to be operated to conversions of greater than 90 percent total unsaturates. As best as can be determined, the formyl composition disclosed in
US 3,787,459 consists of from 24 to 92 percent monoformyl and from 17 to 75 percent
10 diformyl products.

Other prior art, such as EP-B1-711748, discloses a process for preparing di- and polyformylcarboxylic esters by hydroformylation of esters of multiply unsaturated fatty acids, such as soybean oil, sunflower oil, linseed oil, and other vegetable oils. The conversion of feedstock appears to range from roughly 55 to 100 percent by weight. The
15 resulting aldehyde composition, as illustrated in the examples, appears to comprise from 23 to 35 percent monoformyl, from 12 to 31 percent diformyl, and from 3 to 29 percent triformyl products, by weight.

Yet other prior art, illustrated by US 5,177,228, discloses the hydroformylation of an unsaturated fatty acid ester, such as methyl oleate, to a monoformyl
20 fatty acid ester, such as methylformyl stearate.

In view of the above, it would be advantageous to discover aldehyde and alcohol compositions that can be derived from renewable non-petroleum-based feedstocks, such as seed oils. Moreover, it would be advantageous to discover such aldehyde and alcohol compositions that can also be converted into polyols having acceptable properties
25 for use in polyurethane slab stock flexible foam applications.

Summary of the Invention

In a first aspect, this invention provides for a novel aldehyde composition comprising a mixture of formyl-substituted fatty acids or fatty acid esters, which comprises
30 in terms of formyl distribution from greater than about 25 to less than about 95 percent monoformyl, from greater than about 1 to less than about 65 percent diformyl, and from greater than about 0.1 to less than 10 percent triformyl by weight, based on the total weight

of the composition. In addition, the aldehyde composition of this invention is characterized by a diformyl to triformyl weight ratio of greater than about 5/1.

The novel aldehyde composition of this invention can be hydrogenated or aminated to the corresponding alcohol or amine, which is a useful starting material for the preparation of polyols or polyamines, respectively. Polyols and polyamines find utility in the preparation of polyurethane slab stock flexible foams and other polyurethane products. The aldehyde composition of this invention can also be converted into other industrially useful chemicals, including carboxylic acids, hydroxyacids, and amino acids. Advantageously, the aldehyde and alcohol compositions of this invention can be derived from seed oils, which provide for a renewable non-petroleum based raw material feedstock.

In a second aspect, this invention provides for a process of preparing the novel aldehyde composition described hereinabove, comprising contacting a mixture of unsaturated fatty acids or fatty acid esters with carbon monoxide and hydrogen in the presence of a Group VIII transition metal-organophosphine metal salt ligand complex catalyst, and optionally free organophosphine metal salt ligand, under process conditions sufficient to convert greater than about 80 weight percent of the unsaturated fatty acids or fatty acid esters to monoformyl product. (Measurement of conversion is explained in greater detail hereinafter.) In such a manner, a product mixture is obtained of formyl-substituted fatty acids or fatty acid esters comprising in terms of formyl distribution from greater than about 25 to less than about 95 percent monoformyl, from greater than about 1 to less than about 65 percent diformyl, and from greater than about 0.1 to less than 10 percent triformyl products by weight, based on the total weight of the composition. Additionally, the aldehyde composition is characterized by a diformyl to triformyl weight ratio of greater than about 5/1.

In a third aspect, this invention provides for a novel alcohol composition comprising a mixture of hydroxy-substituted fatty acids or fatty acid esters, which comprises in terms of hydroxy distribution from greater than about 25 to less than about 95 percent monoalcohol, from greater than about 1 to less than about 65 percent diol, and from greater than about 0.1 to less than about 10 percent triol by weight, based on the total weight of the composition.

The novel alcohol composition of this invention, advantageously derived from renewable non-petroleum-based seed oil feedstocks, can be used as a starting material

for the preparation of polyols, which find utility in the preparation of polyurethane slab stock flexible foams and other polyurethane products.

In a fourth aspect, this invention provides for a process of preparing the novel alcohol composition described hereinabove, comprising (a) contacting a mixture comprising
5 unsaturated fatty acids or fatty acid esters with carbon monoxide and hydrogen in the presence of Group VIII transition metal-organophosphine metal salt ligand complex catalyst, and optionally free organophosphine metal salt ligand, under conditions sufficient to hydroformylate greater than about 80 weight percent of unsaturated fatty acids or fatty acid esters to monoformyl product, thereby producing a hydroformylation reaction mixture
10 comprising an aldehyde product of formyl-substituted fatty acids or fatty acid esters; (b) separating the aldehyde product from the hydroformylation reaction mixture; and thereafter (c) hydrogenating the aldehyde product with a source of hydrogen in the presence of a hydrogenation catalyst under process conditions sufficient to obtain the alcohol composition comprising a mixture of hydroxy-substituted fatty acids or fatty acid esters, comprising in
15 terms of hydroxy distribution from greater than about 25 to less than about 95 percent monoalcohol, from greater than about 1 to less than about 65 percent diol, and from greater than about 0.1 to less than about 10 percent triol, by weight, based on the total weight of the composition.

20 Detailed Description of the Invention

The inventions described herein allow for beneficial exploitation of naturally occurring and genetically modified seed oils in the preparation of renewable non-petroleum-based chemical feedstocks for use in manufacture of industrial chemicals, preferably, polyurethanes. In a first aspect related thereto, this invention provides for a novel aldehyde
25 composition comprising a mixture of formyl-substituted fatty acids or fatty acid esters comprising in terms of formyl distribution from greater than about 25 to less than about 95 percent monoformyl, from greater than about 1 to less than about 65 percent diformyl, and from greater than about 0.1 to less than about 10 percent triformyl by weight, based on the total weight of the composition. The aldehyde composition is further characterized as
30 comprising a diformyl to triformyl weight ratio of greater than about 5/1. For the purposes of this invention, the term "monoformyl" refers to any fatty acid or fatty acid ester having one formyl (-CHO) substituent. The formyl substituent may occur at any location along the

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no carbon-carbon double or triple bonds present), with the added requirement that the saturates will not contain any formyl or hydroxy substituents (other than those occurring in the natural seed oil).

5 In another more preferred embodiment, the aldehyde composition comprises greater than about 1 percent unsaturates. In another more preferred embodiment, the aldehyde composition comprises less than about 20 percent unsaturates. For the purposes of this invention, the term "unsaturates" refers to any fatty acid or fatty acid ester that contains at least one carbon-carbon double bond, with the added requirement that such compounds will not contain any formyl or hydroxy substituents (other than those occurring in the natural
10 seed oil).

In yet another preferred embodiment, the aldehyde composition comprises less than about 10 weight percent impurities, for example, lactols, lactones, saturated and unsaturated cyclic ethers, and dimer heavies, as described hereinafter.

15 In a second aspect, this invention provides for a process of preparing the novel aldehyde composition described hereinabove, comprising contacting a mixture of unsaturated fatty acids or fatty acid esters with carbon monoxide and hydrogen in the presence of a Group VIII transition metal-organophosphine metal salt ligand complex catalyst, and optionally free organophosphine metal salt ligand, under process conditions sufficient to hydroformylate, typically, greater than about 80 weight percent, and preferably,
20 greater than about 80 weight percent and less than about 99 weight percent, of unsaturated fatty acids or fatty acid esters to monoformyl products, so as to obtain a mixture of formyl-substituted fatty acids or fatty acid esters comprising in terms of formyl distribution from greater than about 25 to less than about 95 percent monoformyl, from greater than about 1 to less than about 65 percent diformyl, and from greater than about 0.1 to less than about 10
25 percent triformyl by weight, based on the total weight of the aldehyde composition, and also having a diformyl to triformyl weight ratio greater than about 5/1.

In a third aspect, this invention provides for a novel alcohol composition comprising a mixture of hydroxy-substituted fatty acids or fatty acid esters comprising in terms of hydroxy distribution from greater than about 25 to less than about 95 percent
30 monoalcohol, from greater than about 1 to less than about 65 percent diol, and from greater than about 0.1 to less than about 10 percent triol by weight, based on the total weight of the composition.

In a preferred embodiment, the alcohol composition comprises greater than about 25 percent, more preferably, greater than about 30 percent monohydroxy-substituted fatty acid(s) or fatty acid ester(s) (monoalcohol), by weight. In a preferred embodiment, the alcohol composition comprises less than about 45 percent, more preferably, less than about 40 percent, monohydroxy-substituted fatty acid(s) or fatty acid ester(s), by weight. In a preferred embodiment, the alcohol composition comprises greater than about 20 percent, and more preferably, greater than about 25 percent dihydroxy-substituted fatty acid(s) or fatty acid ester(s) (diol), by weight. In a preferred embodiment, the alcohol composition comprises less than about 50 percent, and more preferably, less than about 45 percent, dihydroxy-substituted fatty acid(s) or fatty acid ester(s), by weight. In a preferred embodiment, the alcohol composition comprises greater than about 0.5 percent, and more preferably, greater than about 1 percent trihydroxy-substituted fatty acid(s) or fatty acid ester(s) (triol), by weight. In a preferred embodiment, the alcohol composition comprises less than about 5 percent, and more preferably, less than about 4 percent trihydroxy-substituted fatty acid(s) or fatty acid ester(s), by weight. The terms "monoalcohol," "diol," and "triol" refer to fatty acids or fatty acid esters having one, two, or three hydroxy substituents, respectively, at any location along the fatty acid chain. The monoalcohols, diols, and triols may also be saturated or unsaturated.

In a more preferred embodiment, the alcohol composition comprises greater than about 3 percent, even more preferably, greater than about 10 percent, and most preferably, greater than about 15 percent saturates by weight. In a more preferred embodiment, the alcohol composition comprises less than about 35 percent, and most preferably, less than about 30 percent saturates by weight. The term "saturates" is given the same meaning as set forth hereinabove, which includes any fatty acid or fatty acid ester wherein each carbon atom in the fatty acid chain is covalently bonded to four elements (i.e., no carbon-carbon double or triple bonds present), with the added requirement that the saturates do not contain any formyl or hydroxy substituents (except as occur naturally in the seed oil).

In another more preferred embodiment, the alcohol composition comprises less than about 10 percent unsaturates, by weight. The term "unsaturates" will have the same meaning as set forth hereinabove in reference to any fatty acid or fatty acid ester that contains at least one carbon-carbon double bond, with the added requirement that such

components do not contain any formyl or hydroxy substituents (except as may occur in the natural seed oil).

In yet another preferred embodiment, the alcohol composition is characterized by a diol to triol weight ratio of greater than about 5/1, more preferably, greater than about 8/1, and even more preferably, greater than about 10/1.

In yet another preferred embodiment, the alcohol composition comprises less than about 10 weight percent impurities, including lactols, lactones, saturated and unsaturated cyclic ethers, and dimer heavies, as described hereinafter.

In a fourth aspect, this invention provides for a process of preparing the novel alcohol composition described hereinabove, comprising (a) contacting a mixture comprising unsaturated fatty acids or fatty acid esters with carbon monoxide and hydrogen in the presence of a Group VIII transition metal-organophosphine metal salt ligand complex catalyst, and optionally, free organophosphine metal salt ligand, under conditions sufficient to hydroformylate typically greater than about 80 weight percent, and preferably greater than about 80 weight percent and less than about 99 weight percent, unsaturated fatty acids or fatty acid esters to monoformyl products, so as to obtain a hydroformylation reaction mixture comprising an aldehyde product of formyl-substituted fatty acids or fatty acid esters; (b) separating the aldehyde product from the hydroformylation reaction mixture; and thereafter (c) hydrogenating the aldehyde product with a source of hydrogen in the presence of a hydrogenation catalyst under process conditions sufficient to obtain the alcohol composition comprising a mixture of hydroxy-substituted fatty acids or fatty acid esters comprising in terms of hydroxy distribution from greater than about 25 to less than about 95 percent monoalcohol, from greater than about 1 to less than about 65 percent diol, and from greater than about 0.1 to less than about 10 percent triol by weight, based on the total weight of the composition.

The fatty acid or fatty acid ester feedstock suitably employed in preparing the aldehyde and alcohol compositions of this invention is preferably derived from natural and genetically modified (GMO) plant and vegetable seed oils. Suitable non-limiting examples of such seed oils include castor, soybean, olive, peanut, rapeseed, corn, sesame, cottonseed, canola, safflower, linseed, sunflower; high oleic oils; genetically-modified variations of the aforementioned oils; as well as mixtures thereof. Preferably, the fatty acid or fatty acid ester feedstock is derived from soybean (natural and GMO) and sunflower (including high oleic)

oils. More preferably, the fatty acid or fatty acid ester feedstock is derived from natural or genetically modified soybean oils.

Typically, each fatty acid component of the seed oil comprises a fatty acid chain of greater than about 5, preferably, greater than about 10, and more preferably, greater than about 12 carbon atoms. Typically, the fatty acid chain contains less than about 50, preferably, less than about 35, and more preferably, less than about 25 carbon atoms. The fatty acid chain may be straight or branched and substituted with one or more substituents, provided that the substituents do not materially interfere with processes described herein and any desired downstream end-use. Non-limiting examples of suitable substituents include alkyl moieties, preferably, C₁₋₁₀ alkyl moieties, for example methyl, ethyl, propyl, and butyl; cycloalkyl moieties, preferably, C₄₋₈ cycloalkyl; phenyl; benzyl; C₇₋₁₆ alkaryl and aralkyl moieties; hydroxy, ether, keto, and halide (preferably, chloro and bromo) substituents.

Seed oils comprise a mixture of both saturated and unsaturated fatty acids and/or fatty acid esters. For use in this invention, typically, the seed oil comprises greater than about 65 percent, preferably, greater than about 70 percent, and more preferably, greater than about 80 percent unsaturated fatty acids or fatty acid esters. For use in this invention, typically, the seed oil comprises from greater than about 20 to less than about 90 percent mono-unsaturated fatty acids or fatty acid esters; from greater than about 4 to less than about 56 percent di-unsaturated fatty acids or fatty acid esters; and from greater than about 1 to less than about 10 percent tri-unsaturated fatty acids or fatty acid esters, by weight. In seed oils the alcohol segment of the fatty acid ester is glycerol, a trihydric alcohol.

Non-limiting examples of suitable unsaturated fatty acids that may be found in the seed oil feedstock include 3-hexenoic (hydrosorbic), trans-2-heptenoic, 2-octenoic, 2-nonenoic, cis- and trans-4-decenoic, 9-decenoic (caproic), 10-undecenoic (undecylenic), trans-3-dodecenoic (linderic), tridecenoic, cis-9-tetradecenoic (myristoleic), pentadecenoic, cis-9-hexadecenoic (cis-9-palmitoleic), trans-9-hexadecenoic (trans-9-palmitoleic), 9-heptadecenoic, cis-6-octadecenoic (petroselinic), trans-6-octadecenoic (petroselaidic), cis-9-octadecenoic (oleic), trans-9-octadecenoic (elaidic), cis-11-octadecenoic, trans-11-octadecenoic (vaccenic), cis-5-eicosenoic, cis-9-eicosenoic (godoleic), cis-11-docosenoic (cetoleic), cis-13-docosenoic (erucic), trans-13-docosenoic (brassicidic), cis-15-tetracosenoic (selacholeic), cis-17-hexacosenoic (ximenic), and cis-21-triacontenoic (lumequeic) acids, as

well as 2,4-hexadienoic (sorbic), cis-9-cis-12-octadecadienoic (linoleic), cis-9-cis-12-cis-15-octadecatrienoic (linolenic), eleostearic, 12-hydroxy-cis-9-octadecenoic (ricinoleic), cis-5-docosenoic, cis-5,13-docosadienoic, 12,13-epoxy-cis-9-octadecenoic (vernolic), and 14-hydroxy-cis-11-eicosenoic acid (lesquerolic) acids. The most preferred unsaturated fatty acid is oleic acid.

Generally, the fatty acid ester feedstock employed in preparing the aldehyde or alcohol compositions of this invention is obtained by transesterifying a seed oil with a lower alkanol. Transesterification produces the corresponding mixture of saturated and unsaturated fatty acid esters of the lower alkanol. Because glycerides can be difficult to process and separate, transesterification of the seed oil with a lower alkanol yields mixtures that are more suitable for chemical transformations and separation. Typically, the lower alcohol has from 1 to about 15 carbon atoms. The carbon atoms in the alcohol segment may be arranged in a straight-chain or branched structure, and may be substituted with a variety of substituents, such as those previously disclosed hereinabove in connection with the fatty acid segment, provided that such substituents do not interfere with processing and downstream applications. Preferably, the alcohol is a straight-chain or branched C₁₋₈ alkanol, more preferably, a C₁₋₄ alkanol. Even more preferably, the lower alkanol is selected from methanol, ethanol, and isopropanol. Most preferably, the lower alkanol is methanol.

Any known transesterification method can be suitably employed, provided that the ester products of the lower alkanol are achieved. The art adequately discloses transesterification (e.g., methanolysis, ethanolysis) of seed oils; for example, refer to WO 2001/012581, DE 19908978, and BR 953081. Typically, in such processes, the lower alkanol is contacted with alkali metal, preferably sodium, at a temperature between about 30°C and about 100°C to prepare the corresponding metal alkoxide. Then, the seed oil is added to the alkoxide mixture, and the resulting reaction mixture is heated at a temperature between about 30°C and about 100°C until transesterification is effected. The crude transesterified composition may be separated from the reaction mixture by methods known in the art, including for example, phase separation, extraction, and/or distillation. The crude product may also be separated from co-products and/or decolorized using column chromatography, for example, with silica gel. Variations on the above procedure are documented in the art.

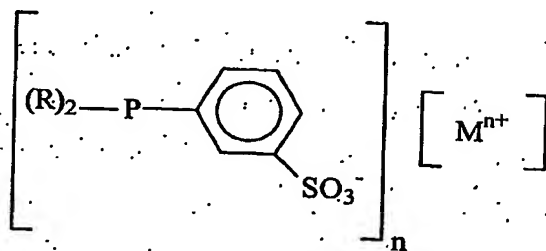
If a mixture of fatty acids, rather than fatty acid esters, is desirably employed as the feedstock for this invention, then the selected seed oil can be hydrolyzed to obtain the corresponding mixture of fatty acids. Methods for hydrolyzing seed oils to their constituent fatty acids are also well known in the art.

5 In the process to prepare the aldehyde composition of this invention, the mixture of fatty acids or fatty acid esters, preferably derived from a seed oil, is subjected to hydroformylation. It is preferred to employ non-aqueous hydroformylation processes that employ the operational features taught in US patents 4,731,486 and 4,633,021, especially those taught in US 4,731,486; the disclosures of said patents being incorporated herein by
10 reference. Accordingly, another aspect of this invention comprises contacting the mixture of unsaturated fatty acids or fatty acid esters, preferably derived from a seed oil, with carbon monoxide and hydrogen in a non-aqueous reaction medium in the presence of a solubilized Group VIII transition metal-organophosphine metal salt ligand complex catalyst, and optionally solubilized free organophosphine metal salt ligand, under conditions sufficient to
15 prepare the aldehyde composition described herein. The term "non-aqueous reaction medium" means that the reaction medium is essentially free of water, which means that to the extent that water is present at all, it is not present in an amount sufficient to cause the hydroformylation reaction mixture to be considered as encompassing a separate aqueous or water phase or layer in addition to the organic phase. The term "free" organophosphine
20 metal salt ligand means that the organophosphine metal salt ligand is not complexed, that is, not bound or tied to the Group VIII transition metal.

The Group VIII transition metals are meant to be selected from the group consisting of iron (Fe), cobalt (Co), nickel (Ni), ruthenium (Ru), rhodium (Rh), palladium (Pd), osmium (Os), iridium (Ir), and platinum (Pt); and mixtures thereof; with the preferred
25 metals being rhodium, ruthenium, cobalt, and iridium; more preferably, rhodium and cobalt; and most preferably, rhodium. The oxidation state of the Group VIII metal may be any available oxidation state, either electronically neutral (zero) or electronically deficient (positive valence), that allows for bonding to the organophosphine ligand. Moreover, the oxidation state of the Group VIII transition metal, as well as the overall oxidation state of
30 the complex or any complex precursor, may vary under the hydroformylation process conditions. The term "complex" as used herein shall be taken to mean a coordination compound formed by the union of one or more organophosphine ligands with the Group

VIII transition metal. The number of available coordination sites on the Group VIII transition metal is well known in the art and may range typically from about 4 to about 6. Optionally, the Group VIII transition metal may be additionally bonded to carbon monoxide, hydrogen, or both carbon monoxide and hydrogen. In general, the Group VIII transition metal is employed in the hydroformylation process in a concentration range of from about 10 parts per million (ppm) to about 1000 ppm, by weight, calculated as free metal. In rhodium catalyzed hydroformylation processes, it is generally preferred to employ from about 10 to about 800 ppm of rhodium calculated as free metal.

The organophosphine metal salt ligand preferably employed in the hydroformylation process of this invention comprises a monosulfonated tertiary phosphine metal salt, preferably, represented by formula I hereinafter:



(I)

wherein each R group individually represents a radical containing from 1 to about 30 carbon atoms selected from the classes consisting of alkyl, aryl alkaryl, aralkyl, and cycloalkyl radicals; wherein M represents a metal cation selected from the group consisting of alkali and alkaline earth metals; and wherein n has a value of 1 or 2 corresponding to the valence of the particular metal cation M. Non-limiting examples of monosulfonated tertiary phosphine metal salt ligands of the aforementioned structure are illustrated in the art, for example, in US 4,731,486, incorporated herein by reference. More preferred ligands are selected from monosulfonated metal salt derivatives of triphenylphosphine, diphenylcyclohexylphosphine, phenyldicyclohexylphosphine, tricyclohexylphosphine, diphenylisopropylphosphine, phenyldiisopropylphosphine, diphenyl-t-butylphosphine, phenyldi-t-butylphosphine, and the like. A most preferred ligand is selected from the monosulfonated metal salt derivatives of phenyldicyclohexylphosphine.

The hydroformylation process of this invention may be conducted in an excess amount of free ligand, for example, at least one mole of free monosulfonated tertiary

organophosphine metal salt ligand per mole of Group VIII transition metal present in the reaction medium. In general, amounts of free ligand from about 2 to about 300, and preferably, from about 5 to about 200 moles per mole of Group VIII transition metal present in the reaction medium should be suitable for most purposes, particularly with regard to rhodium catalyzed processes. If desired, make-up organophosphine ligand can be supplied to the reaction medium or the hydroformylation process at any time and in any suitable manner, so as to maintain preferred concentrations of free ligand in the reaction medium.

The monosulfonated tertiary phosphine metal salt ligands mentioned hereinabove are generally water soluble, and not soluble or very poorly soluble in most olefins and/or aldehydes, and particularly, not soluble or very poorly soluble in the unsaturated fatty acids or fatty acid esters and formyl derivatives thereof under consideration in this invention. It is known, however, that by use of certain organic solubilizing agents, the monosulfonated tertiary phosphine metal salt ligand and Group VIII complexes thereof can be rendered organically soluble and thus employable in non-aqueous hydroformylation reaction media. Organic solubilizing agents used for the aforementioned purpose are disclosed in the prior art, for example, in US 5,180,854 and US 4,731,486, incorporated herein by reference. US 5,180,854 discloses as organic solubilizing agents amides, glycols, sulfoxides, sulfones, and mixtures thereof. N-methyl-2-pyrrolidinone (NMP) is one preferred organic solubilizing agent. As disclosed in US 4,731,586, other suitable polar solvents or solubilizing agents include alkylene oxide oligomers having an average molecular weight greater than about 150 up to about 10,000, and higher; organic nonionic surfactant mono-ols having an average molecular weight of at least about 300; and alcohol alkoxylates containing both water-soluble (polar) and oil-soluble (non-polar) groups readily available under the trade names TERGITOLS™ (The Dow Chemical Company).

The reaction conditions for effecting the non-aqueous hydroformylation process can be those heretofore conventionally used. A reaction temperature typically greater than about 45°C, and preferably, greater than about 60°C can be suitably employed. The hydroformylation process, however, typically operates at a temperature less than about 200°C, and preferably, less than about 130°C. Such a process generally operates at a pressure greater than about 1 psia (6.9 kPa), preferably, greater than about 50 psia (345 kPa). Typically, the process operates at a pressure less than about 10,000 psia (69 MPa), preferably, less than about 1,500 psia (10 MPa), and more preferably, less than about 500

psia (3.5 MPa). The minimum total pressure of the reactants is not particularly critical and depends predominately on the amount and nature of the reactants employed to obtain a desired rate of reaction. More specifically, the carbon monoxide partial pressure is preferably greater than about 1 psia (6.9 kPa), and more preferably, greater than about 25 psia (172 kPa). The carbon monoxide partial pressure is preferably less than about 150 psia (1,034 kPa), and more preferably, less than about 120 psia (827 kPa). The hydrogen partial pressure preferably is greater than about 10 psia (69 kPa), more preferably, greater than about 25 psia (172 kPa). The hydrogen partial pressure is preferably less than about 150 psia (1,034 kPa), and more preferably, less than about 120 psia (827 kPa). In general, the molar ratio of gaseous hydrogen to carbon monoxide ($H_2:CO$) can range from about 1:10 to about 10:1. The reaction medium residence time typically ranges from greater than about 1 hour to less than about 40 hours per reactor. The hydroformylation process can be operated as a batch process, or preferably, conducted as a continuous process with recycle of the complex catalyst and optional free ligand. A preferred reactor comprises from 1 to about 3 continuous stirred tank reactors connected in series. Other engineering variations are known and described in the art.

The conversion of unsaturated fatty acid(s) and/or fatty acid ester(s) can be conveniently measured, for example, by gas phase chromatographic (gc) methods known to those of skill in the art. More specifically, a gc peak or peaks representative of the unsaturated fatty acids or fatty acid esters (i.e., compounds with no formyl substituents) is typically found to decrease in peak height and peak area as the hydroformylation progresses. The extent of this peak loss can be correlated with the conversion of unsaturated fatty acids or fatty acid esters first to monoformyl-substituted products. Some monoformyl products containing additional unsaturation will be involved in a secondary reaction to diformyl products; and some diformyl products containing additional unsaturation will be involved in a tertiary reaction to triformyl products. For the purposes of this invention, these secondary and tertiary reactions to diformyl and triformyl products are not considered in the calculation of conversion. Consideration is given only to the conversion of the first unsaturated bond per molecule of unsaturated fatty acid or fatty acid ester to monoformyl product. Under the process conditions described hereinbefore, the hydroformylation process is conducted to a conversion of greater than about 80 weight percent unsaturated fatty acids or fatty acid esters. Preferably, the conversion is greater than about 85 weight percent

unsaturated fatty acids or fatty acid esters. Preferably, the conversion is less than about 99 weight percent, and more preferably, less than about 95 weight percent unsaturated fatty acids or fatty acid esters, based on the conversion of one unsaturated bond per molecule. Note that by the instant definition the conversion is not equivalent to converting greater than 80 percent of *all* unsaturated bonds.

When the hydroformylation process is conducted as described hereinabove, then an aldehyde composition is obtained that comprises a mixture of formyl-substituted fatty acids or fatty acid esters having the following composition by weight: from greater than about 25 to less than about 95 percent monoformyl, from greater than about 1 to less than about 65 percent diformyl, and from greater than about 0.1 to less than about 10 percent triformyl-substituted fatty acids or fatty acid esters; preferably, from greater than about 3 to less than about 20 percent saturates; preferably, from greater than about 1 to less than about 20 percent unsaturates; and preferably, less than about 10 percent impurities, by weight. In addition, the aldehyde composition exhibits a diformyl to triformyl weight ratio typically greater than about 5/1, preferably, greater than about 8/1, and more preferably, greater than about 10/1. Typically, the diformyl to triformyl weight ratio is less than about 250/1.

The formyl-substituted fatty acids or fatty acid esters may contain impurities including but not limited to lactols, lactones, unsaturated cyclic ethers, saturated cyclic ethers, and dimer heavies. Commonly found species of lactols, lactones, unsaturated cyclic ethers, saturated cyclic ethers, and dimer heavies are illustrated in Figure 1 for a C_{18} carbon chain. Analogous species may be present based on fatty acids or fatty acid esters of chain length different from 18. Typically, the concentration of lactols and/or lactones is greater than about 0.01 weight percent. Typically, the concentration of lactols and/or lactones is less than about 20; and preferably, less than about 10 weight percent, based on the total weight of the aldehyde composition. Typically, the concentration of unsaturated and/or saturated cyclic ethers is greater than about 0.01 weight percent. Typically, the concentration of unsaturated and/or saturated cyclic ethers is less than about 10 weight percent, based on the total weight of the aldehyde composition. Typically, the concentration of dimer heavies is greater than about 0.01 weight percent. Typically, the concentration of dimer heavies is less than about 10 weight percent, based on the total weight of the aldehyde composition. Typically, the total concentration of impurities, for example, lactols, lactones,

saturated and unsaturated cyclic ethers, and dimer heavies, is greater than about 0.01 percent, by weight. Preferably, the total concentration of impurities, for example, lactols, lactones, saturated and unsaturated cyclic ethers, and dimer heavies, is less than about 10 percent, preferably, less than about 5 percent, and more preferably, less than about 2 percent by weight, based on the total weight of the aldehyde composition. Generally, it is desirable to maintain a low level of these impurities, because their presence may impact the properties of manufactured downstream end-products.

The aldehyde composition can be separated by methods known in the art from the hydroformylation reaction medium, the Group VIII transition metal-organophosphine metal salt ligand complex catalyst, and free organophosphine metal salt ligand. Extraction is a preferred method of separation. A suitable extraction method is described in US 5,180,854, incorporated herein by reference. The extraction method disclosed therein comprises mixing the non-aqueous reaction mixture with from about 2 to about 60 percent by weight of added water and from 0 to about 60 percent by weight of a non-polar hydrocarbon, and then by phase separation forming a non-polar phase consisting essentially of the aldehyde composition and the non-polar hydrocarbon compound, if any, and a liquid polar phase consisting essentially of water, the Group VIII transition metal-organophosphine metal salt ligand complex catalyst, optionally free organophosphine metal salt ligand, and any organic solubilizing agent. Typically, the non-polar hydrocarbon comprises a saturated straight chain alkane containing from about 6 to about 30 carbon atoms, such as, hexane.

As a result of the above-described hydroformylation and separation procedures, the aldehyde composition may additionally comprise small quantities of water, hydroformylation solvent, solubilizing agent, and/or extraction solvent.

The conversion of aldehydes to alcohols is known in the art, and such conventional methods can be applied to convert the aldehyde composition of this invention to the alcohol composition of this invention. Typically, the aldehyde composition comprising the mixture of formyl-substituted fatty acids or fatty acid esters is contacted with a source of hydrogen in the presence of a hydrogenation catalyst under hydrogenation process conditions sufficient to prepare the alcohol composition of hydroxy-substituted fatty acids or fatty acid esters. The source of hydrogen may be pure hydrogen or hydrogen diluted with a non-reactive gas, such as nitrogen, helium, argon, a saturated hydrocarbon, or

the like. The hydrogenation catalyst comprises typically a Group VIII transition metal, preferably selected from palladium, platinum, rhodium, and nickel, which may be supplied as Raney metal or as supported metal on a suitable catalyst support, such as carbon or silica. A preferred hydrogenation catalyst is Raney nickel. The hydrogenation may be conducted neat or in a solution of a suitable hydrocarbon solvent. The temperature for such hydrogenations is generally greater than about 50°C, and preferably, greater than about 80°C. The temperature for such hydrogenations is typically less than about 250°C, and preferably, less than about 175°C. The hydrogen pressure is generally greater than about 50 psig (345 kPa). The hydrogen pressure is generally less than about 1,000 psig (6,895 kPa), and preferably, less than about 500 psig (3,447 kPa).

The hydrogenation conducted as described hereinabove produces the alcohol composition comprising a mixture of hydroxy-substituted fatty acids or fatty acid esters comprising in terms of hydroxy distribution from greater than about 25 to less than about 95 percent monoalcohol, from greater than about 1 to less than about 65 percent diol, and from greater than about 0.1 to less than about 10 percent triol; preferably, from greater than about 3 to less than about 35 percent saturates; and preferably, from greater than about 0.01 to less than about 10 percent unsaturates. The alcohol composition may optionally contain impurities, such as lactols, lactones, saturated and unsaturated cyclic ethers, and dimer heavies, preferably having the structures shown in Figure 1 for a fatty acid of carbon chain length 18 or analogous structures for fatty acids of different chain length. Typically, the concentrations of lactols, lactones, saturated and unsaturated cyclic ethers, and dimer heavies are the same as those set forth hereinabove in connection with the aldehyde composition. Typically, the total concentration of lactols, lactones, saturated and unsaturated cyclic ethers, and dimer heavies is greater than about 0.01 weight percent. Preferably, the total concentration of lactols, lactones, saturated and unsaturated cyclic ethers, and dimer heavies is less than about 10 percent, preferably, less than about 5 percent, and more preferably, less than about 2 percent by weight, based on the total weight of the alcohol composition. The alcohol composition is further characterized as typically comprising a diol to triol weight ratio of greater than about 5/1, preferably, greater than about 8/1, and more preferably, greater than about 10/1. Generally, the diol to triol weight ratio is less than about 250/1.

The alcohol composition disclosed herein may be oligomerized in the presence of a catalytic initiator to form oligomeric polyol compositions that find utility in the preparation of polyurethane slab stock flexible foam applications. Representative process conditions for the alcohol oligomerization and description of the polyols derived therefrom may be found in US provisional patent application serial no. _____ (Attorney's Docket no. 62260), filed concurrently herewith, in the names of *Zenon Lysenko et al.* and entitled "Improved Process to Make Vegetable Oil-Based Polyols and Polyols Made Therefrom," which application is incorporated herein by reference. The oligomeric polyol compositions thus prepared generally possess an average molecular weight in the range from about 600 to about 6,000. Polyurethanes prepared with these oligomeric polyols possess acceptable properties, including acceptable cross-link density, for use in slab stock flexible foams. Details of the manufacture of such foams and description of their properties may also be found in the aforementioned co-pending US patent application.

The following examples are presented hereinbelow to illustrate the inventions described herein. The examples should not be construed to limit the inventions in any manner. Based on the description provided herein, variations and modifications of the examples will be apparent to those of skill in the art.

Example 1.

A catalyst solution was prepared by dissolving dicarbonylacetylacetonato rhodium (I) (0.078 g) and dicyclohexyl-(3-sulfonylphenyl)phosphine mono-sodium salt (0.7513g) in n-methyl-2-pyrrolidinone (NMP) (53.8934 g) under a nitrogen atmosphere. A portion of the resulting mixture (11.06 g) was then transferred to a nitrogen-purged 100 mL stainless steel autoclave and heated to 90°C under 200 psig (1,379 kPa) of synthesis gas (1:1 hydrogen:carbon monoxide) with mixing via mechanical agitation at 700 rpm. The mixture was heated for about 15 minutes. To this mixture was added under synthesis gas soy methyl esters (38.98 g) comprising by weight 9 percent methyl palmitate, 5 percent methyl stearate, 24 percent methyl oleate, 51 percent methyl linoleate, and 8 percent methyl linolenate. The reactor pressure was maintained at 400 psig (2,758 kPa) by the addition of fresh synthesis gas. The mixture was analyzed after 22.5 hours of reaction time. The resulting unsaturated ester conversion and aldehyde composition are shown below in Table 1.

Table 1. Aldehyde Compositions Derived from Hydroformylation of Soy Methyl Esters

Ex.	% Conv	Saturates	Unsat	Monoformyl	Diformyl	Triformyl	Heavies	Di/Tri Ratio
1	84	14	14	40	30	2	0.2	15/1
2	88	14	10	37	37	2	1.3	18/1
3	98	14	2	33	48	4	0.3	12/1
4	95	14	4	34	44	4	0.5	11/1

5 Example 2.

The procedure described in Example 1 was repeated with the following modifications: catalyst solution (10.92 g) and soy methyl esters (39.19 g). Temperature was maintained at 90°C and pressure at 400 psig (2,758 kPa). After 20 hours of reaction time an aldehyde composition obtained from the reaction mixture was analyzed with the results shown in Table 1.

10 Example 3.

A catalyst solution was prepared by dissolving dicarbonylacetylacetonato rhodium (I) (0.080 g) and dicyclohexyl-(3-sulfonylphenyl)phosphine mono-sodium salt (0.3514 g) in n-methyl-2-pyrrolidinone (NMP) (54.059 g) under a nitrogen atmosphere. A portion of the resulting mixture (11.17 g) was then transferred to a nitrogen-purged 100 mL stainless steel autoclave and heated to 90°C under 200 psig (1,379 kPa) of synthesis gas (1:1 hydrogen:carbon monoxide) with mixing via mechanical agitation at 700 rpm. The mixture was heated for about 15 minutes. To this mixture was added under synthesis gas soy methyl esters (39.09 g) comprising by weight 9 percent methyl palmitate, 5 percent methyl stearate, 24 percent methyl oleate, 51 percent methyl linoleate, and 8 percent methyl linolenate. The reactor pressure was maintained at 400 psig (2,758 kPa) by the addition of fresh synthesis gas. The mixture was analyzed after 25.5 hours of reaction time. The resulting unsaturated ester conversion and aldehyde composition are shown in Table 1.

Example 4.

The procedure described in Example 3 was repeated with the following modifications. The catalyst solution (11.08 g) and soy methyl ester (38.49 g) were transferred to the reactor where the temperature was maintained at 70°C and the pressure at 400 psig for 20 hours. The resulting unsaturated ester conversion and aldehyde composition are shown in Table 1.

Example 5.

An up-flow tubular reactor was packed with a commercial supported nickel catalyst (440 mL, Sud-Chemie C46-8-03). The inlet of the reactor was comprised of two liquid feeds and one gas feed that came together before entering the reactor. The two liquid feeds consisted of a hydroformylated soy methyl ester (saturates 13 percent, mono-aldehyde 34.3 percent, dialdehyde 45.1 percent, trialdehyde 1.5 percent) and recycled hydrogenation product from the same aldehyde supply. The flow rate of the hydroformylated soy methyl ester was 5 g/min; the flow rate of the recycled hydrogenation product was 19 g/min. Total Liquid Hourly Space Velocity was 3.51 hr⁻¹. Hydrogen gas was fed to the reactor at 2,000 sccm (Gas Hourly Space Velocity 272 hr⁻¹), and the reactor was heated to 143°C. Pressure was set at 830 psig (5,723 kPa). Analysis of the mixture after hydrogenation yielded the alcohol composition described in Table 2.

Table 2. Alcohol Compositions Derived from Hydrogenation of Formyl-Substituted Fatty Acid Esters^{1,2}

Example	Saturates	Mono-ol	Diol	Triol	Dimer Heavies	Lactones	Ethers
5	18.8	34.7	37.8	3.2	2.5	0.2	0.32
6	23.8	35.0	34.7	2.3	1.6	0.6	nd
7	30.6	38.2	25.3	1.3	2.6	0.5	0.1

1. Nd = Not detected.

2. Unsaturates not detected in any of Examples 5 to 7.

Example 6.

Hydrogenation was conducted on a formylated feed using the reactor design and catalyst described in Example 5. The two liquid feeds consisted of a hydroformylated soy methyl ester (saturates 13.8 percent, mono-aldehyde 35.4 percent, dialdehyde 39.8 percent, trialdehyde 0.6 percent) and recycled hydrogenation product from the same aldehyde supply. The flow rate of the hydroformylation soy methyl ester was 2 g/min; the flow rate of the recycled hydrogenation product was 8 g/min. Total Liquid Hourly Space Velocity was 5.5 hr^{-1} . Hydrogen gas was fed at 1,000 sccm (Gas Hourly Space Velocity 471 hr^{-1}). The reactor was heated to 163°C and maintained at 590 psig (4,068 kPa). Analysis of the mixture after hydrogenation yielded the alcohol composition described in Table 2.

Example 7.

Hydrogenation was conducted on a formylated feed using the reactor design and catalyst described in Example 5. The two liquid feeds consisted of hydroformylated soy methyl ester (saturates 14.2 percent, mono-aldehyde 43 percent, dialdehyde 30.6 percent, trialdehyde 0.4 percent) and recycled hydrogenation product from the same aldehyde supply. The flow rate of the hydroformylated soy methyl ester was 1.89 g/min; the flow rate of the recycled hydrogenation product was 8.2 g/min. Total Liquid Hourly Space Velocity was 5.14 hr^{-1} . Hydrogen gas was fed at 1,000 sccm (Gas Hourly Space Velocity 471 hr^{-1}) and the reactor was heated to 161°C . Pressure was set at 610 psig (4,206 kPa). Analysis of the mixture after hydrogenation yielded the alcohol composition described in Table 2.

Example 8.

In a stainless steel reactor, a solution was prepared containing rhodium (120 parts per million by weight (ppmw)) in the form of dicarbonylacetylacetonato rhodium (I), dicyclohexyl-(3-sulfonylphenyl)phosphine mono-sodium salt (0.3 percent), 1-methyl-2-pyrrolidinone (NMP) (21.6 percent), and soy derived methyl esters (78.1 percent), all percentages by weight. The soy derived methyl esters consisted of 84 percent olefins and 15 percent saturates, by weight. The mixture was placed under 400 psig (2,758 kPa) of synthesis gas (1:1 hydrogen:carbon monoxide) at room temperature, slowly warmed to 90°C , and then maintained at a constant 90°C temperature. During heating the pressure of

the system reached a maximum of 450 psig (3,103 kPa). The pressure was maintained at 400 psig (2,758 kPa) throughout the reaction by the addition of fresh synthesis gas, aside from the pressure increase observed during the initial heating. After reacting for 11 hours, the mixture was sampled for analysis. The mixture was cooled to ambient temperature, nitrogen sparged for about 1 hour, then discharged from the reactor into a container under a nitrogen atmosphere at atmospheric pressure. An aldehyde composition was obtained having the composition shown in Table 3, calculated on the basis of the olefin charged to the system.

Table 3.

Ex.	% Conv.	% Sats	% Unsats	% Mono-formyl	% Di-formyl	% Tri-formyl	Heavies	Di/Tri Ratio
8	98	14	2	31	49	5	0.5	9.8
9	93	14	6	35	41	4	0.2	10.3
10	92	14	7	34	41	4	0.2	10.3
11	92	14	6	34	41	4	0.2	10.3
12	92	14	6	34	42	4	0.4	10.5

Examples 9-11.

The procedure of Example 8 was repeated three times as Examples 9, 10, and 11, with the modification of a reaction time of 5.5 hours. Aldehyde compositions were obtained, as shown in Table 3.

Example 12.

The procedure of Example 8 was repeated with the modification of a reaction time of 6 hours. An aldehyde composition was obtained, as shown in Table 3.

Example 13.

The aldehyde compositions obtained from Examples 9, 10, and 11 were combined, mixed with water at 70°C (water was 60 percent by weight of the total organic mass). The mixture was allowed to settle and the organic layer separated from the aqueous layer. The organic layer was washed four additional times with water, in each instance the water layer was removed from the organic layer after allowing the phases to separate. Analysis of the organic layer after washing showed that 98 percent of the rhodium and

1

Table 4.

Component	Composition (% by wt)
Saturates + Olefins	20
Monoaldehyde	34
Dialdehyde	40
Trialdehyde	4
Heavies	0.3
NMP	0.1
<i>Di/Tri Ratio</i>	<i>10/1</i>

5 The hydroformylated soy methyl ester composition (50 g), obtained from the
above extraction, and Raney® Nickel 2400 (1.5 g, Grace Davison) were charged into a
pressure reactor under air and the reactor was sealed. Nitrogen (100 psig, 689 kPa) was
slowly pressurized into the reactor and then released slowly. This was repeated three times
to replace the air in the reactor with nitrogen. The reactor was purged hydrogen. The reactor
10 was then stirred at 844 rpm with mechanical agitation, and heated to 120°C under 400 psig
(2,758 kPa) of hydrogen. The reactor was then fed with hydrogen to maintain reaction
pressure at 400 psig (2,758 kPa). Analysis of the mixture after 24.1 hours of reaction time
yielded the alcohol composition described in Table 5.

Table 5.

Component	Alcohol Composition (Wt. %)
Saturates + Olefins	19
Monoalcohol	34
Diol	40
Triol	4
Heavies	1.2
Lactones	0.5
Ethers	Nd ¹

1. ND = Not detected.

WHAT IS CLAIMED IS:

1. An aldehyde composition comprising a mixture of formyl-substituted fatty acids or fatty acid esters comprising in terms of formyl distribution from greater than about 25 to less than about 95 percent monoformyl, from greater than about 1 to less than about 65 percent diformyl, and from greater than about 0.1 to less than about 1.0 percent triformyl by weight, based on the total weight of the composition, and further comprising a diformyl to triformyl weight ratio of greater than about 5/1.
2. The aldehyde composition of Claim 1 further comprising from greater than about 3 to less than about 20 percent saturates, by weight.
3. The aldehyde composition of Claim 1 or 2 further comprising from greater than about 1 to less than about 20 percent unsaturates, by weight.
4. The aldehyde composition of Claim 1 wherein the diformyl to triformyl weight ratio is greater than about 10/1.
5. The aldehyde composition of Claim 1 comprising less than about 10 weight percent total impurities selected from lactols, lactones, saturated cyclic ethers, unsaturated cyclic ethers, and dimer heavies.
6. The aldehyde composition of Claim 1 comprising from greater than about 25 to less than about 45 percent monoformyl, from greater than about 20 to less than about 50 percent diformyl, and from greater than about 0.5 to less than about 5 percent triformyl substituted fatty acids or fatty acid esters, by weight.
7. The aldehyde composition of Claim 1 comprising from greater than about 30 to less than about 40 percent monoformyl, from greater than about 25 to less than about 45 percent diformyl, and from greater than about 1 to less than about 2.6 percent triformyl substituted fatty acids or fatty acid esters, by weight.
8. The aldehyde composition of Claim 1 being prepared by a process comprising contacting a mixture of unsaturated fatty acids or fatty acid esters with carbon monoxide and hydrogen in the presence of a Group VIII transition metal-organophosphine metal salt ligand complex catalyst, and optionally free organophosphine metal salt ligand, under process conditions sufficient to convert greater than about 80 weight percent of unsaturated fatty acids or fatty acid esters to monoformyl products.

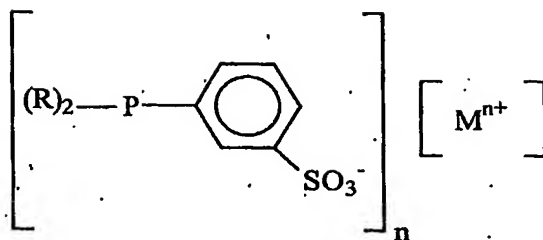
9. The composition of Claim 8 wherein the mixture of unsaturated fatty acids or fatty acid esters is derived from a seed oil.

10. The composition of Claim 8 wherein the seed oil is selected from naturally occurring and genetically modified seed oils of the group consisting of castor, soybean, olive, peanut, rapeseed, corn, sesame, cottonseed, canola, safflower, linseed, sunflower, including high oleic oils, and mixtures thereof.

11. The composition of Claim 8 wherein the temperature is greater than about 45°C and less than about 200°C, and wherein the pressure is greater than about 1 psia (6.9 kPa) and less than about 10,000 psia (69 MPa).

12. A process of preparing an aldehyde composition comprising contacting a mixture of unsaturated fatty acids or fatty acid esters with carbon monoxide and hydrogen in the presence of a Group VIII transition metal-organophosphine metal salt ligand complex catalyst, and optionally free organophosphine metal salt ligand, under process conditions sufficient to hydroformylate greater than about 80 weight percent of the unsaturated fatty acids or fatty acid esters to monoformyl products, so as to produce a mixture of formyl-substituted fatty acids or fatty acid esters comprising in terms of formyl distribution from greater than about 25 to less than about 95 percent monoformyl, from greater than about 1 to less than about 65 percent diformyl, and from greater than about 0.1 to less than 10 percent triformyl by weight, based on the total weight of the composition, and having a diformyl to triformyl weight ratio of greater than about 5/1.

13. The process of Claim 12 wherein the ligand is a monosulfonated tertiary organophosphine represented by the following formula:



wherein each R group individually represents a radical containing from 1 to about 30 carbon atoms; wherein M represents a metal cation selected from the group consisting of alkali and alkaline earth metals; and wherein n has a value of 1 or 2 corresponding to the valence of the particular metal cation M.

14. The process of Claim 13 wherein the ligand is selected from the group consisting of the monosulfonated metal salts of triphenylphosphine, diphenylcyclohexylphosphine, phenyldicyclohexylphosphine, tricyclohexylphosphine, diphenylisopropylphosphine, phenyldiisopropylphosphine, diphenyl-t-butylphosphine, phenyldi-t-butylphosphine, and mixtures thereof.

15. The process of Claim 12 wherein the Group VIII transition metal of the complex catalyst is selected from rhodium, ruthenium, cobalt, iridium, and mixtures thereof.

16. The process of Claim 12 wherein the temperature is greater than about 45°C and less than about 200°C; and wherein the pressure is greater than about 1 psia (6.9 kPa) and less than about 10,000 psia (69 MPa).

17. An alcohol composition comprising a mixture of hydroxy-substituted fatty acids or fatty acid esters comprising in terms of hydroxy distribution from greater than about 25 to less than about 95 percent mono alcohol, from greater than about 1 to less than about 65 percent diol, and from greater than about 0.1 to less than about 10 percent triol by weight, based on the total weight of the composition.

18. The alcohol composition of Claim 17 further comprising from greater than about 3 to less than about 35 percent saturates.

19. The alcohol composition of Claim 17 or 18 further comprising from greater than about 0.01 to less than about 10 percent unsaturates.

20. The alcohol composition of Claim 17 having a diol to triol weight ratio of greater than about 5/1.

5 21. The alcohol composition of Claim 17 comprising less than about 10 weight percent total impurities selected from the group consisting of lactols, lactones, saturated cyclic ethers, unsaturated cyclic ethers, and dimer heavies.

22. The alcohol composition of Claim 17 comprising from greater than about 25 to less than about 45 percent monoalcohol, from greater than about 20 to less than about 50 percent diol, and from greater than about 0.5 to less than about 5 percent triol substituted fatty acids or fatty acid esters, by weight.

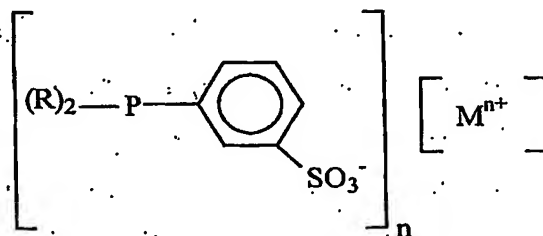
23. The alcohol composition of Claim 17 comprising from greater than about 30 to less than about 40 percent monoalcohol, from greater than about 25 to less than about 45 percent diol, and from greater than about 1 to less than about 4 percent triol substituted fatty acids or fatty acid esters, by weight.

24. The alcohol composition of Claim 17 being prepared by a process comprising (a) contacting a mixture comprising unsaturated fatty acids or fatty acid esters with carbon monoxide and hydrogen in the presence of a Group VIII transition metal-organophosphine metal salt ligand complex catalyst, and optionally, free organophosphine metal salt ligand, under conditions sufficient to hydroformylate greater than about 80 weight percent of the unsaturated fatty acids or fatty acid esters to monoformyl products, so as to obtain a hydroformylation reaction mixture comprising an aldehyde composition of formyl-substituted fatty acids or fatty acid esters; (b) separating the aldehyde composition from the hydroformylation reaction mixture; and thereafter (c) hydrogenating the aldehyde composition with a source of hydrogen in the presence of a hydrogenation catalyst under process conditions sufficient to obtain the alcohol composition.

25. A process of preparing an alcohol composition comprising (a) contacting a mixture comprising unsaturated fatty acids or fatty acid esters with carbon monoxide and hydrogen in the presence of a Group VIII transition metal-organophosphine metal salt ligand complex catalyst, and optionally, free organophosphine metal salt ligand, under conditions sufficient to hydroformylate greater than about 80 weight percent of unsaturated fatty acids or fatty acid esters to monoformyl products, so as to obtain a hydroformylation reaction

mixture comprising an aldehyde product of formyl-substituted fatty acids or fatty acid esters; (b) separating the aldehyde product from the hydroformylation reaction mixture; and thereafter (c) hydrogenating the aldehyde product with a source of hydrogen in the presence of a hydrogenation catalyst under process conditions sufficient to obtain the alcohol composition comprising a mixture of hydroxy-substituted fatty acids or fatty acid esters comprising in terms of hydroxy distribution from greater than about 25 to less than about 95 percent mono alcohol, from greater than about 1 to less than about 65 percent diol, and from greater than about 0.1 to less than about 10 percent triol by weight, based on the total weight of the composition.

26. The process of Claim 25 wherein the ligand is a monosulfonated tertiary organophosphine represented by the following formula:



- wherein each R group individually represents a radical containing from 1 to about 30 carbon atoms; wherein M represents a metal cation selected from the group consisting of alkali and alkaline earth metals; and wherein n has a value of 1 or 2 corresponding to the valence of the particular metal cation M.

27. The process of Claim 26 wherein the ligand is selected from the group consisting of the monosulfonated salts of triphenylphosphine, diphenylcyclohexylphosphine, phenyldicyclohexylphosphine, tricyclohexylphosphine, diphenylisopropylphosphine, phenyldiisopropylphosphine, diphenyl-t-butylphosphine, phenyl-di-t-butylphosphine, and mixtures thereof.

28. The process of Claim 25 wherein the Group VIII transition metal is selected from rhodium, ruthenium, cobalt, iridium, and mixtures thereof.

29. The process of Claim 25 wherein the hydroformylation is conducted at a temperature of greater than about 45°C and less than about 200°C and a pressure greater than about 1 psia (6.9 kPa) and less than about 10,000 psia (69 MPa).

5 30. The process of Claim 25 wherein the aldehyde composition is separated from the hydroformylation reaction mixture by extraction.

31. The process of Claim 25 wherein the hydrogenation catalyst is Raney nickel.

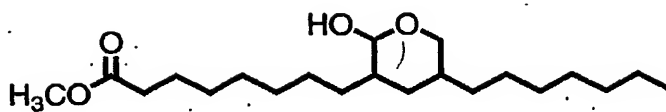
10 32. The process of Claim 25 wherein the hydrogenation is conducted at a temperature greater than about 50°C and less than about 250°C and at a pressure greater than about 50 psig (345 kPa) and less than about 1,000 psia (6,895 kPa).

ABSTRACT OF THE DISCLOSURE

An aldehyde composition derived by hydroformylation of a transesterified seed oil and containing a mixture of formyl-substituted fatty acids or fatty acid esters having the following composition by weight: greater than about 25 to less than about 95 percent monoformyl, greater than about 1 to less than about 65 percent diformyl, and greater than about 0.1 to less than about 10 percent triformyl-substituted fatty acids or fatty acid esters, and having a diformyl to triformyl weight ratio of greater than about 5/1; preferably, greater than about 3 to less than about 20 percent saturates; and preferably, greater than about 1 to less than about 20 percent unsaturates. An alcohol composition derived by hydrogenation of the aforementioned aldehyde composition, containing a mixture of hydroxy-substituted fatty acids or fatty acid esters having the following composition by weight: greater than about 25 to less than about 95 percent monoalcohol, greater than about 1 to less than about 65 percent diol, greater than about 0.1 to less than about 10 percent triol-substituted fatty acids or fatty acid esters; preferably greater than about 3 to less than about 35 percent saturates; and preferably, greater than about 0.01 to less than about 10 percent unsaturates. The alcohol composition can be converted into an oligomeric polyol for use in the manufacture of polyurethane slab stock flexible foams.

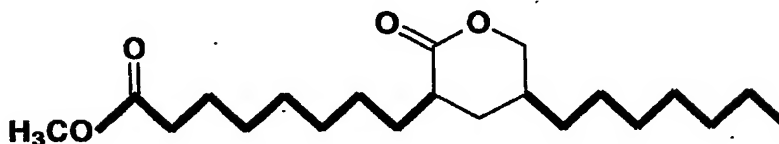
FIGURE 1

LACTOL



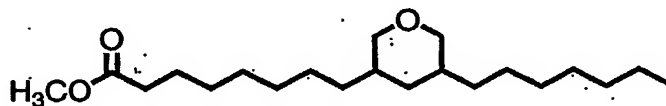
$C_{21}H_{40}O_4$
Mol. Wt.: 356.54

LACTONE



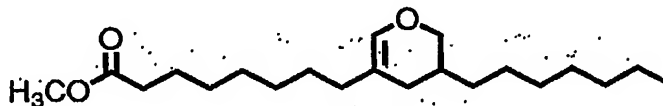
$C_{21}H_{38}O_4$
Mol. Wt. 354.53

SATURATED CYCLIC ETHER



$C_{21}H_{40}O_3$
Mol. Wt.: 340.54

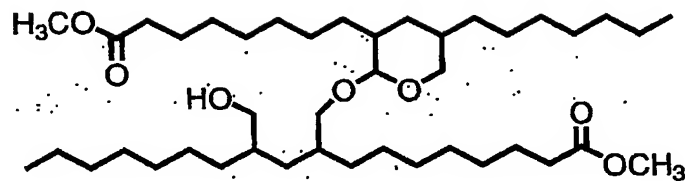
UNSATURATED CYCLIC ETHER



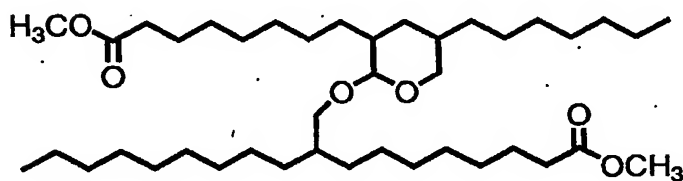
$C_{21}H_{38}O_3$
Mol. Wt.: 338.52

63104

DIMER HEAVIES



C₄₂H₈₀O₇
Mol. Wt.: 697.08



C₄₁H₇₈O₆
Mol. Wt.: 667.05

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